

# Inverse problems in a microchannel

## *The correlation method*

Tutorial 6 - Christophe Ravey , C.Pradere



I2M Departement TREFLE, CNRS UB1

Esplanade des Arts et Métiers

33405 Talence Cedex, France

### Research Areas:

- Fluids and Flows
- Transfers and Porous Media
- Energy and Thermal Systems

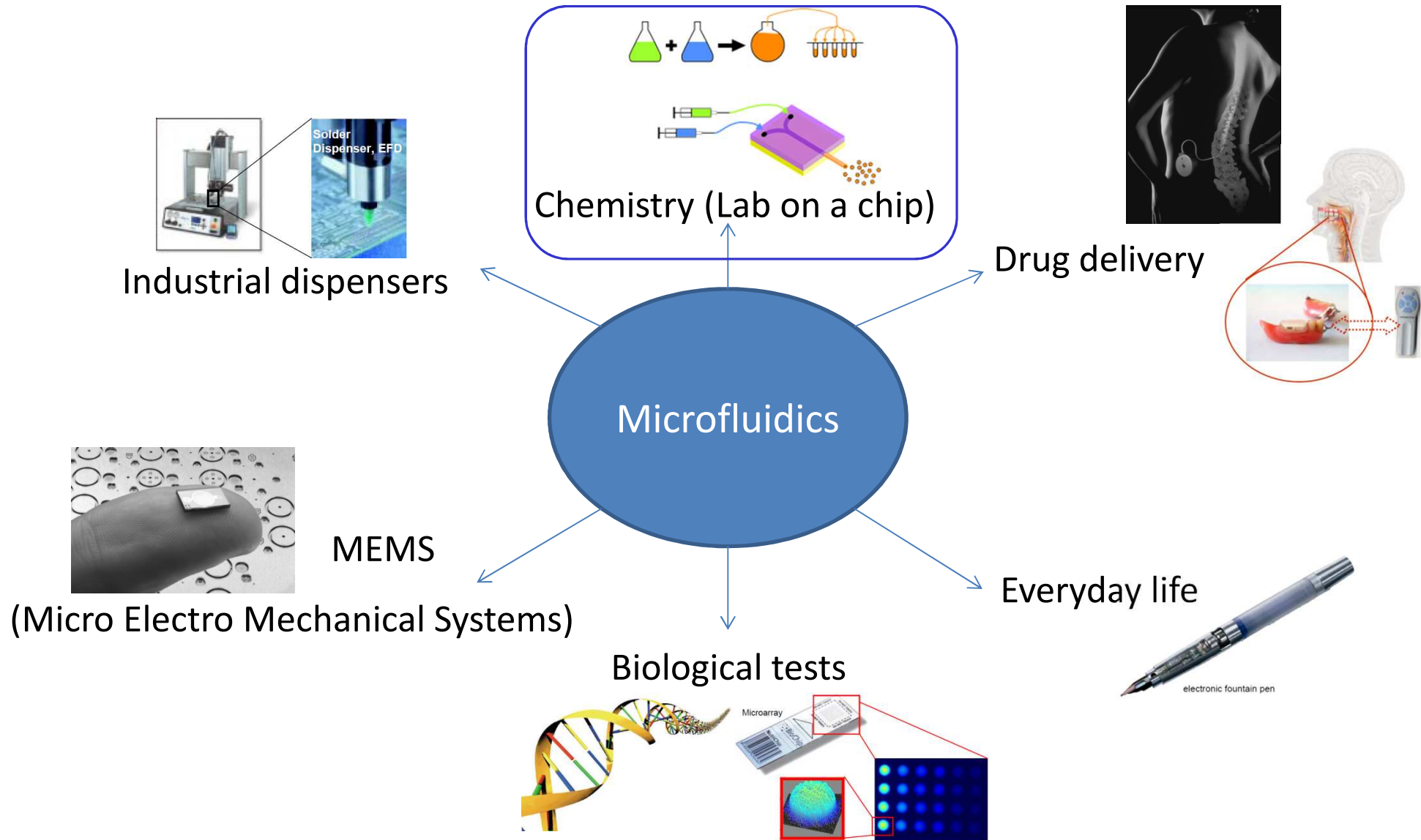
- 1. Objectives of this tutorial**
2. Microfluidics systems
3. Experimental Setup
4. Modeling of a microfluidics system
5. The correlation method
6. Some experimental work
7. Results
8. Conclusion

## Main goal : presentation of the correlation method

- Description of the experimental bench
  - Microfluidics*
  - IR Thermography*
- Perform real time treatment
  - Matlab*
- See the application of the method to different topics
  - Flow characterization*
  - Source term detection (chemical reaction or phase change)*

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## Stakes and challenges



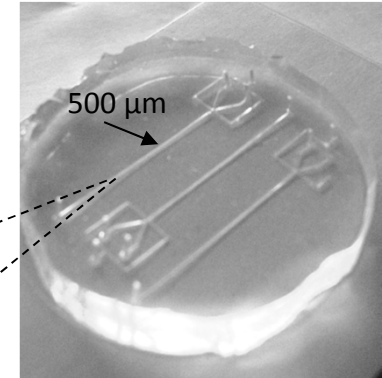
## Thermal characterization

**Field of application: chemical reaction (Rhodia)**

Chemical, pharmaceutical, medical industries...

**Challenge**

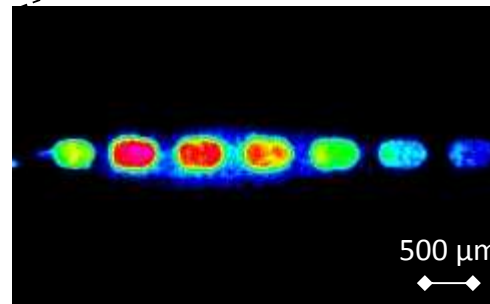
Controlling the reaction  
Data acquisition  
Safety



*Microfluidics chip*

**Thermochemical properties in microfluidics**

Thermodynamics and  
kinetics data  
Reactor design



*Acid/base droplets reaction, film 600 fps*

**Thermal analysis tool**

Scale ( $\approx 25 \mu\text{m}$ )

Quantitative measurements

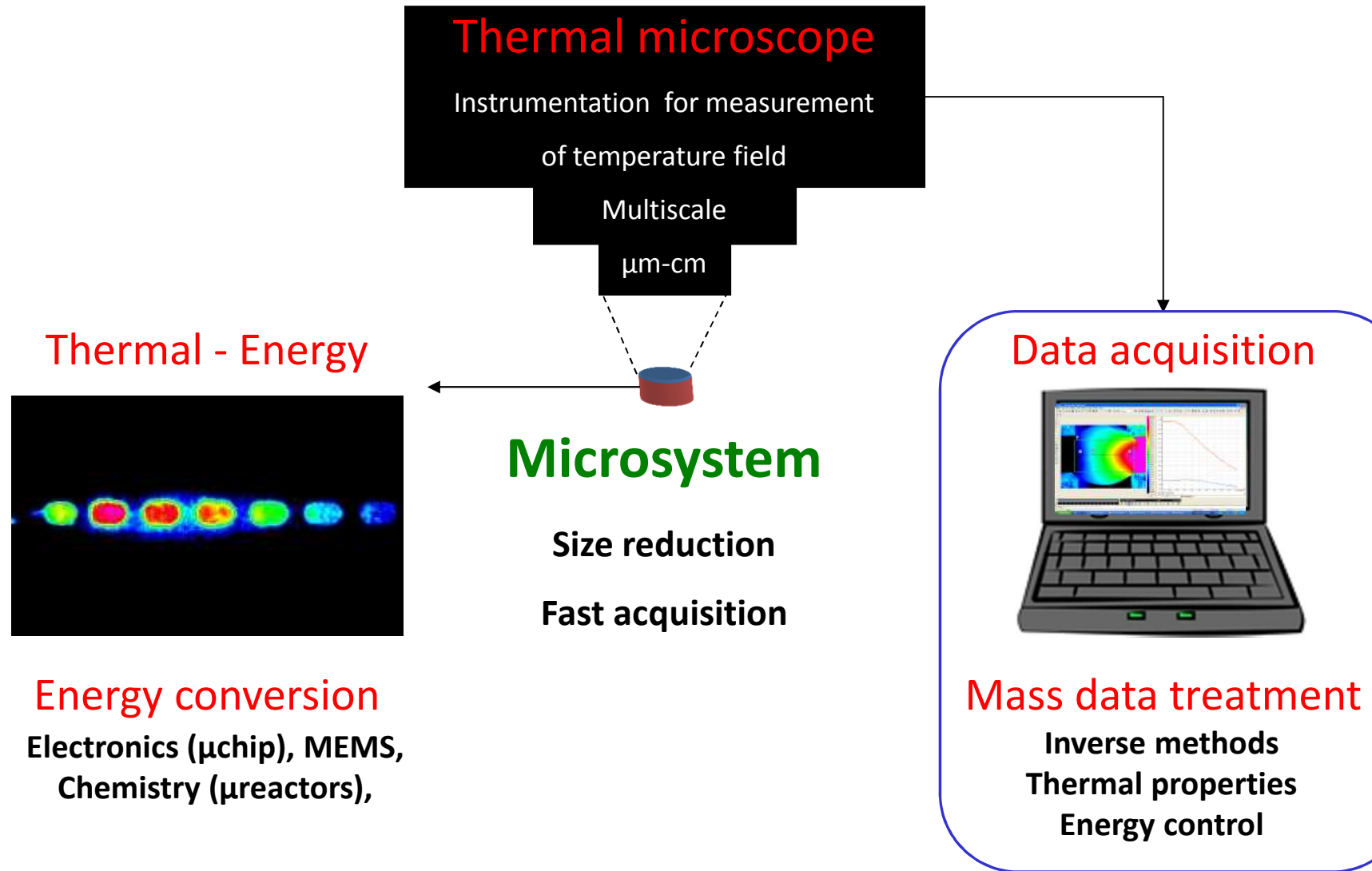
( $\approx \mu\text{W}$ , mK, ms)

**Difficulties :**

Instrumentations, inverse methods

**Heterogeneous, small sizes, volumes and heat flux...**

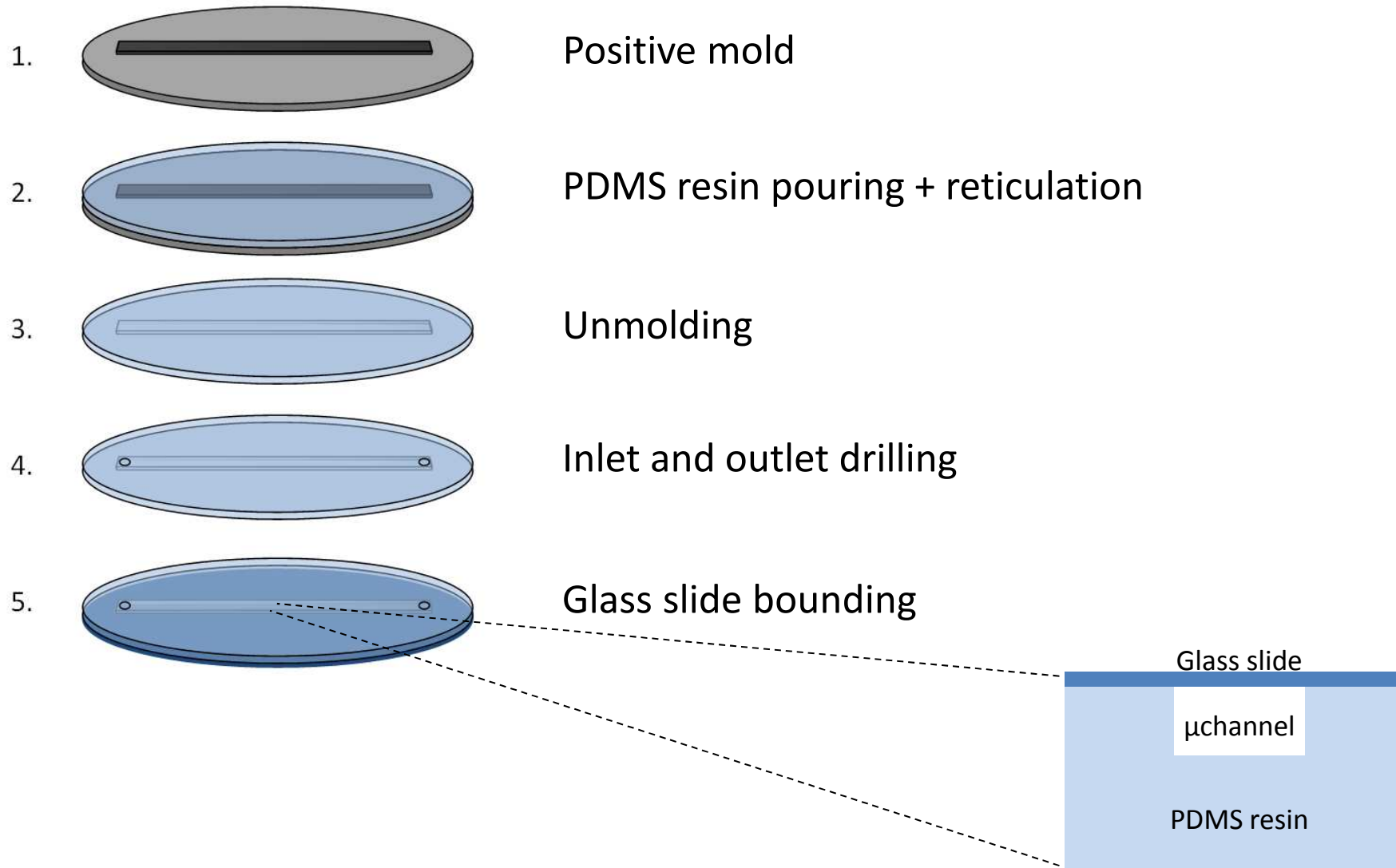
## InfraRed Thermography



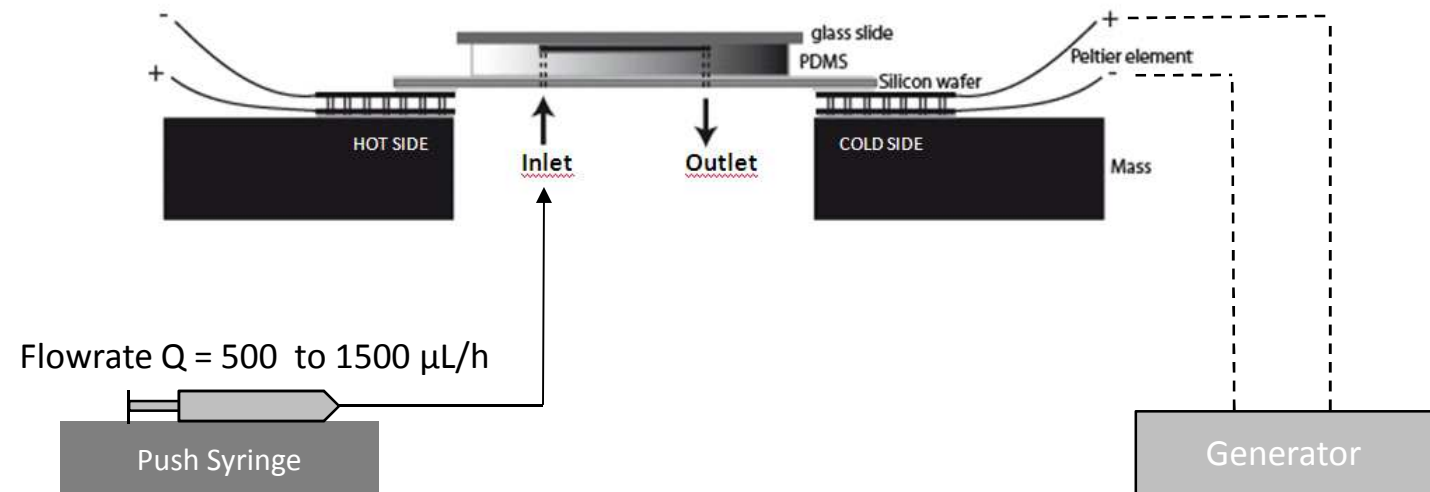
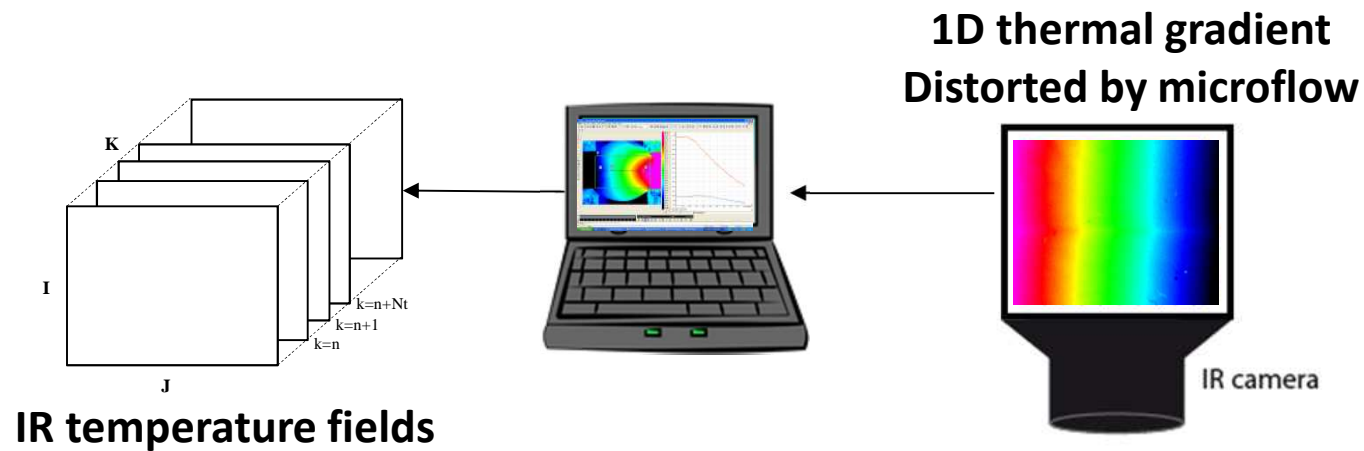
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## Microfluidics chip

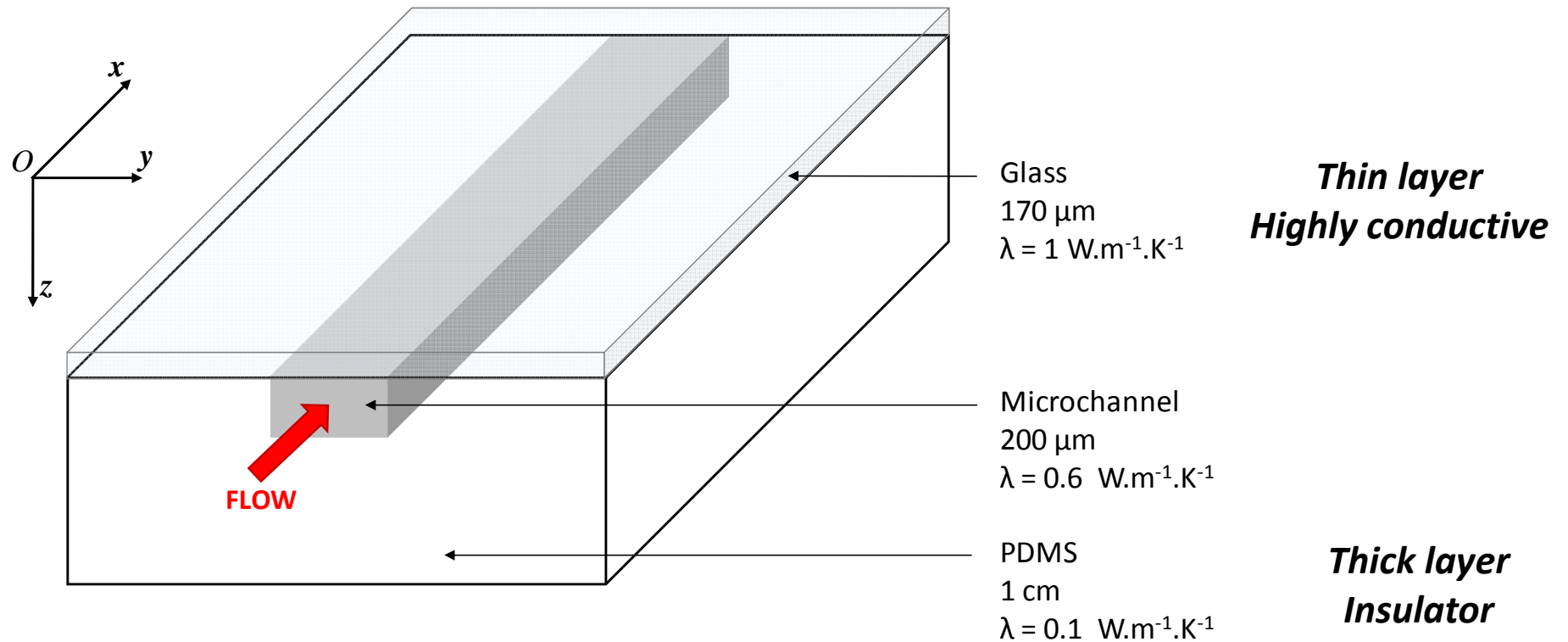


## InfraRed Thermography for microfluidics systems



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## 3D scheme of used microfluidics chip

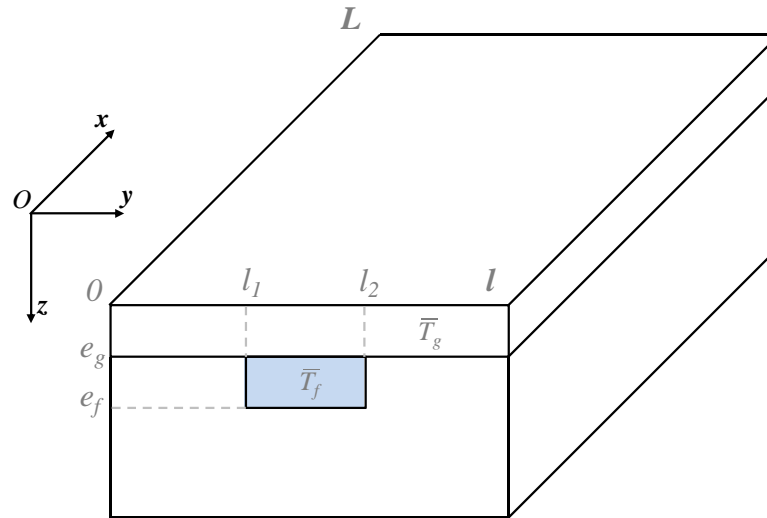


### Assumptions:

Geometry, thermal properties of layers, flow  $\Rightarrow$  2D model (x,y) for IR measurements

Averaged over z direction

## Heat equation inside the microchannel



$$\bar{T}_f(x, y, t) = \int_{e_g}^{e_f} T_f(x, y, z, t) dz$$

$$\left| \lambda_f \frac{\partial T_f(x, y, z, t)}{\partial z} \right|_{e_g}^{e_f} + e_f \bar{\phi}_f(x, y, t) + \lambda_f e_f \left( \frac{\partial^2 \bar{T}_f(x, y, t)}{\partial x^2} + \frac{\partial^2 \bar{T}_f(x, y, t)}{\partial y^2} \right) = \rho_f c p_f e_f \left( v(x, y, t) \frac{\partial \bar{T}_f(x, y, t)}{\partial x} + \frac{\partial \bar{T}_f(x, y, t)}{\partial t} \right)$$

### Boundary conditions

$$-\lambda_f \frac{\partial \bar{T}_f(x, y, t)}{\partial x} = \phi_C \text{ for } x = 0 \text{ and } -\lambda_f \frac{\partial \bar{T}_f(x, y, t)}{\partial x} = \phi_F \text{ for } x = L$$

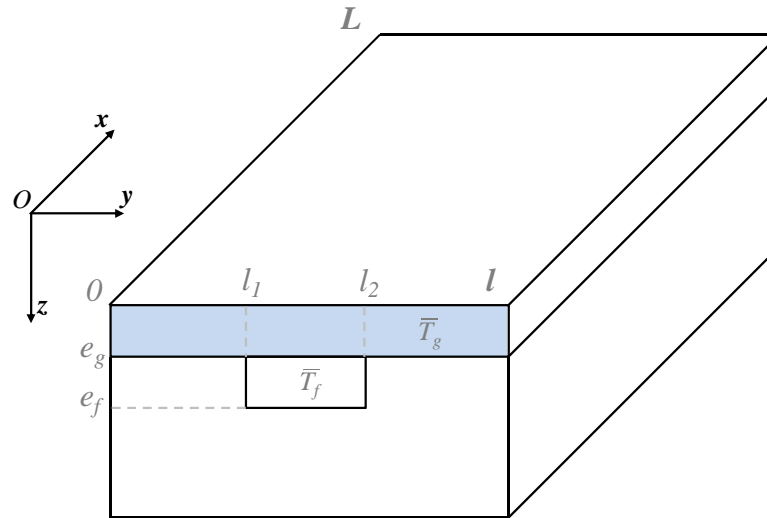
$$\bar{T}_f(x, y, t) = 0 \text{ for } t = 0$$

$$\frac{\partial \bar{T}_f(x, y, t)}{\partial y} = 0 \text{ for } y = l_1 \text{ and } y = l_2$$

$$-\lambda_f \frac{\partial T_f(x, y, z, t)}{\partial z} = -\lambda_g \frac{\partial T_g(x, y, z, t)}{\partial z} \text{ for } z = e_g$$

$$\frac{\partial T_f(x, y, z, t)}{\partial z} = 0 \text{ for } z = e_f$$

## Heat equation inside the glass plate



$$\overline{T}_g(x, y, t) = \int_0^{e_g} T_g(x, y, z, t) dz$$

$$\left| \lambda_g \frac{\partial T_g(x, y, z, t)}{\partial z} \right|_0^{e_g} + \lambda_g e_g \left( \frac{\partial^2 \overline{T}_g(x, y, t)}{\partial x^2} + \frac{\partial^2 \overline{T}_g(x, y, t)}{\partial y^2} \right) = \rho_g c p_g e_g \frac{\partial \overline{T}_g(x, y, t)}{\partial t}$$

## Boundary conditions

$$-\lambda_g \frac{\partial \overline{T}_g(x, y, t)}{\partial x} = \phi_c \text{ for } x = 0 \text{ and } -\lambda_g \frac{\partial \overline{T}_g(x, y, t)}{\partial x} = \phi_F \text{ for } x = L$$

$$-\lambda_f \frac{\partial T_f(x, y, z, t)}{\partial z} = -\lambda_g \frac{\partial T_g(x, y, z, t)}{\partial z} \text{ for } z = e_g$$

$$\frac{\partial \overline{T}_g(x, y, t)}{\partial y} = 0 \text{ for } y = 0 \text{ and } y = l$$

$$-\lambda_g \frac{\partial T_g(x, y, z, t)}{\partial z} = h T_g(x, y, z, t) \text{ for } z = 0$$

$$\overline{T}_g(x, y, t) = 0 \text{ for } t = 0$$

## Overall heat equation

Local thermal equilibrium between the averaged temperatures :  $\overline{T_g} = \overline{T_f} = T$

$$-h T(x, y, 0, t) + e_f \overline{\varphi_f}(x, y, t) + (\lambda_f e_f + \lambda_g e_g) \left( \frac{\partial^2 T(x, y, t)}{\partial x^2} + \frac{\partial^2 T(x, y, t)}{\partial y^2} \right) = \rho_f c p_f e_f v(x, y, t) \frac{\partial T(x, y, t)}{\partial x} + (\rho_f c p_f e_f + \rho_g c p_g e_g) \frac{\partial T(x, y, t)}{\partial t}$$

Finite differences

$$H_{i,j}^k T_{i,j}^k + \Phi_{i,j}^k + \Delta T_{i,j}^k = Pe^{*k}_{i,j} T x_{i,j}^k + \left( \frac{1}{Fo^{*k}_{i,j}} \right) T t_{i,j}^k$$

$$\Delta T_{i,j}^k + \Phi_{i,j}^k = Pe^{*k}_{i,j} T x_{i,j}^k + \left( \frac{1}{Fo^{*k}_{i,j}} \right) T t_{i,j}^k$$

$$Pe^{*k}_{i,j} = K1 \cdot \frac{v_{i,j}^k \Delta l}{a_{f,i,j}^k} \quad \text{and} \quad K1 = \frac{1}{\left( 1 + \frac{\lambda_g e_g}{\lambda_f e_f} \right)} \quad Fo^{*k}_{i,j} = K2 \cdot \frac{a_{f,i,j}^k \Delta t}{\Delta l^2} \quad \text{and} \quad K2 = \frac{\left( 1 + \frac{\lambda_g e_g}{\lambda_f e_f} \right)}{\left( 1 + \frac{\rho_g c p_g e_g}{\rho_f c p_f e_f} \right)}$$

$$H_{i,j}^k = \frac{h_{i,j}^k \Delta l^2}{(\lambda_f e_f + \lambda_g e_g)}, \quad \Phi_{i,j}^k = \frac{e_f \overline{\varphi_{i,j}^k} \Delta l^2}{(\lambda_f e_f + \lambda_g e_g)}$$

$$T x_{i,j}^k = (T_{i+1,j}^k - T_{i,j}^k), \quad T t_{i,j}^k = (T_{i,j}^{k+1} - T_{i,j}^k)$$

$$\Delta T_{i,j}^k = (T_{i+1,j}^k + T_{i-1,j}^k + T_{i,j+1}^k + T_{i,j-1}^k - 4T_{i,j}^k)$$

## Overall heat equation

$$\Delta T_{ij}^k + \Phi_{ij}^k = Pe_{ij}^k T x_{ij}^k + \left( \frac{1}{Fo_{ij}^k} \right) (t_{ij}^k)$$

What we measure :

$T$

What we want :

$\Phi$

$Pe$

$Fo$



Source term



velocity



Thermal  
diffusivity

## Play with the model

create different operating conditions in order to estimate different parameters.



## “Step by step” approach

### Without heat source

Steady state

$$\Delta T_{i,j}^k = Pe^{*k} T x_{i,j}^k$$

*Calibration of  $Pe$*

Transient state flow OFF

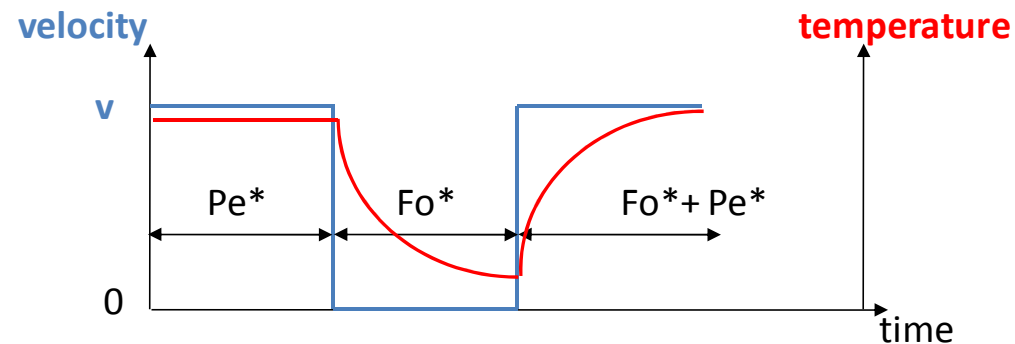
$$\Delta T_{i,j}^k = \left( \frac{1}{Fo^{*k}} \right) T t_{i,j}^k$$

*Calibration of  $Fo$*

Transient state flow ON

$$\Delta T_{i,j}^k = Pe^{*k} T x_{i,j}^k + \left( \frac{1}{Fo^{*k}} \right) T t_{i,j}^k$$

*Calibration of  $Fo$  and  $Pe$*



### With heat source

Steady state

$$\Delta T_{i,j}^k + \Phi_{i,j}^k = Pe^{*k} T x_{i,j}^k$$

*Estimation of  $Pe$  and  $\Phi$*

Transient state

$$\Delta T_{i,j}^k + \Phi_{i,j}^k = Pe^{*k} T x_{i,j}^k + \left( \frac{1}{Fo^{*k}} \right) T t_{i,j}^k$$

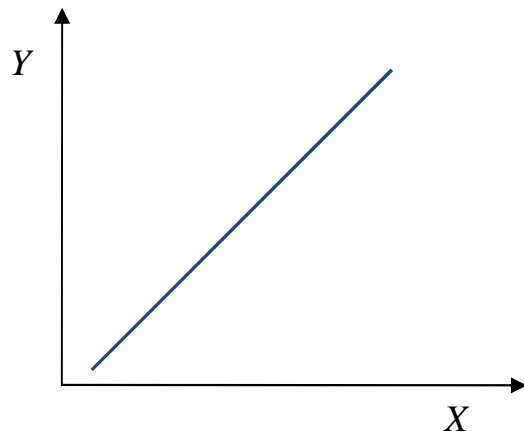
*Estimation of  $Pe$ ,  $Fo$  and  $\Phi$*

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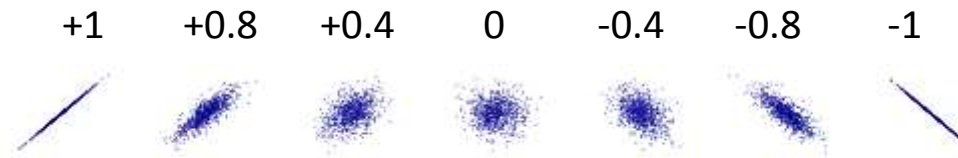
## The correlation coefficient: S

Example with steady state, no heat source:

$$\Delta T_{i,j}^k = Pe^{*k} T x_{i,j}^k \longrightarrow Y = A \cdot X$$



Correlation between Y and X: 
$$S_{Y,X} = \frac{\Sigma(Y - \bar{Y}) \cdot (X - \bar{X})}{\sqrt{\Sigma(Y - \bar{Y})^2} \cdot \sqrt{\Sigma(X - \bar{X})^2}}$$



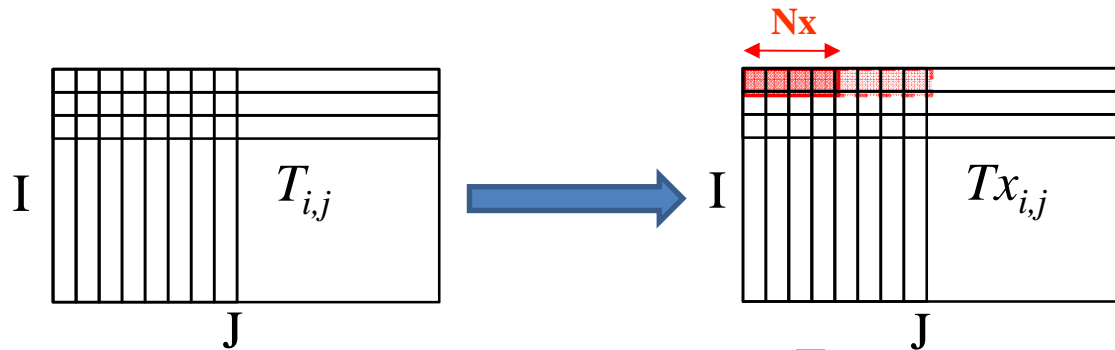
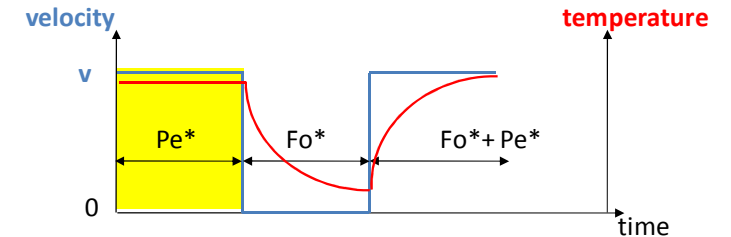
On the same principle, correlation between  $\Delta T$  and  $Tx$

$$S_{X_{i,j}} = \frac{\Sigma_{j=n}^{n+Nx} \Delta T_{i,j} \cdot T x_{i,j}}{\sqrt{(\Sigma_{j=n}^{n+Nx} \Delta T_{i,j})^2} \cdot \sqrt{(\Sigma_{j=n}^{n+Nx} T x_{i,j})^2}}$$

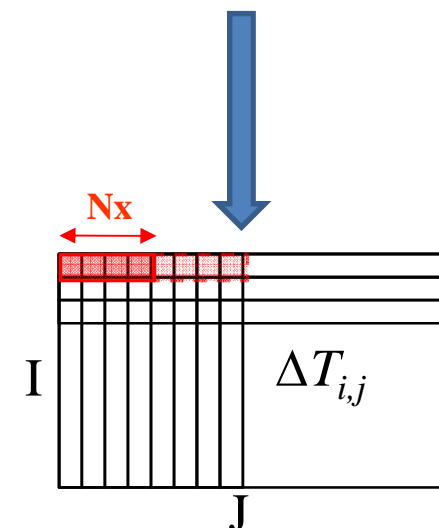
=> Look for values of +1, meaning the model is valid

## The spatial correlation coefficient

Steady state, no heat source :  $\Delta T_{i,j}^k = Pe_{i,j}^k Tx_{i,j}^k$

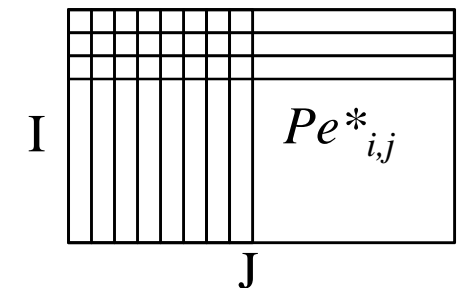


Spatial correlation between  $\Delta T$  and  $T_x$



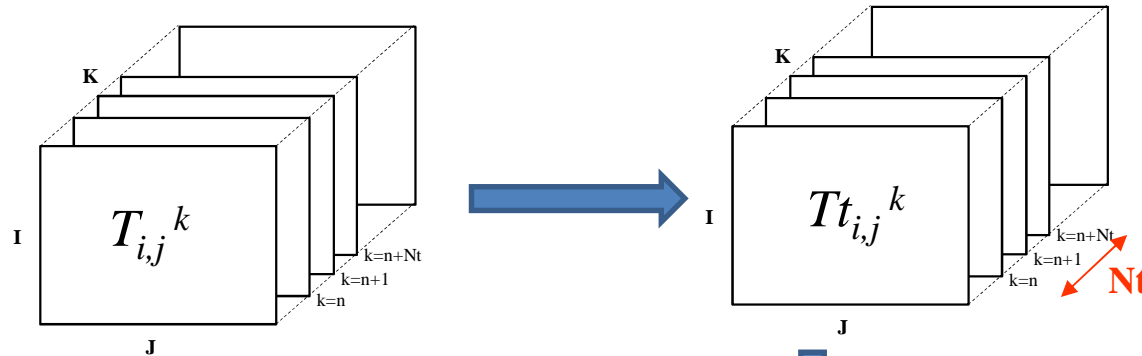
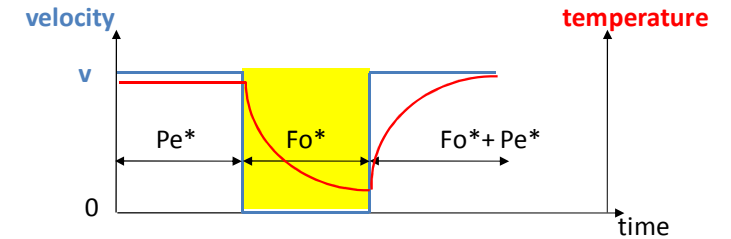
$$Sx_{i,j} = \frac{\sum_{j=n}^{n+Nx} \Delta T_{i,j} \cdot Tx_{i,j}}{\sqrt{(\sum_{j=n}^{n+Nx} \Delta T_{i,j})^2} \cdot \sqrt{(\sum_{j=n}^{n+Nx} Tx_{i,j})^2}} \quad \text{for } n \in [1; (J - Nx)]$$

$$\text{if } Sx_{i,j} = 1 \quad Pe_{i,j}^* = Sx_{i,j} \frac{\sqrt{(\sum_{j=n}^{n+Nx} \Delta T_{i,j})^2}}{\sqrt{(\sum_{j=n}^{n+Nx} Tx_{i,j})^2}}$$

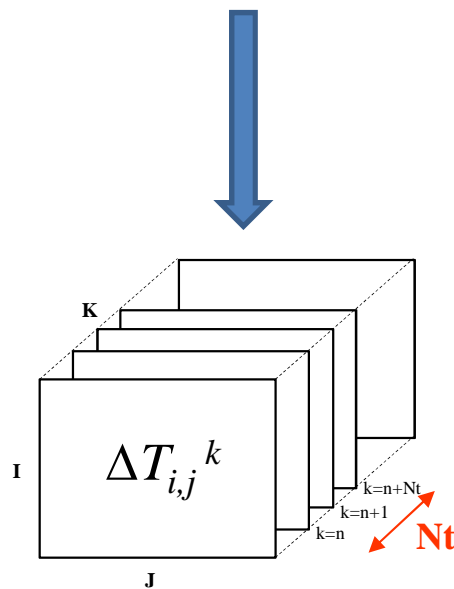


## The temporal correlation coefficient

Transient state, no heat source :  $\Delta T_{i,j}^k = \left( \frac{1}{Fo^{*k}_{i,j}} \right) Tt_{i,j}^k$

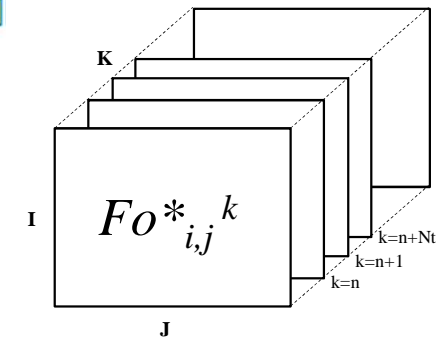


Temporal correlation between  $\Delta T$  and  $Tt$



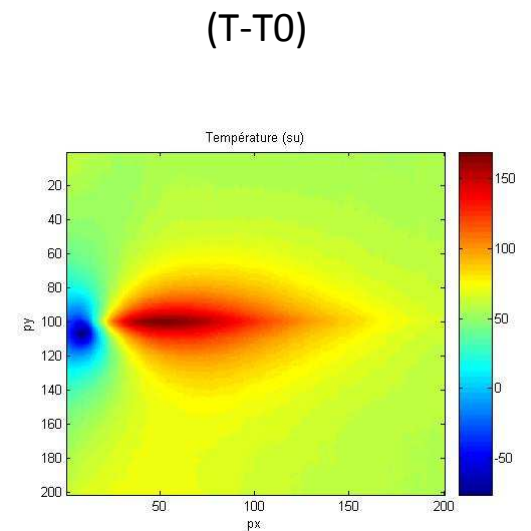
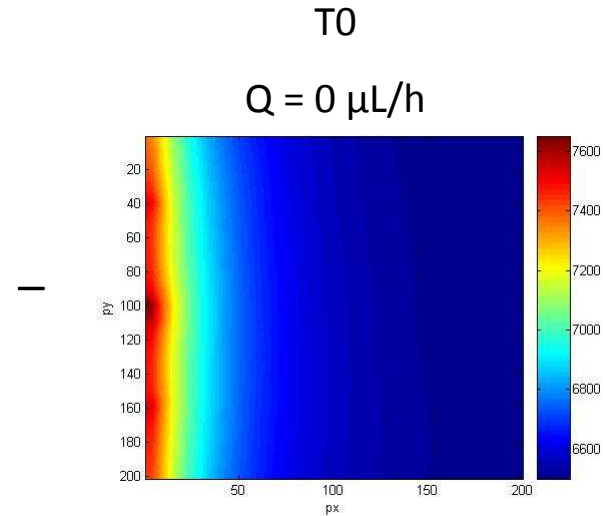
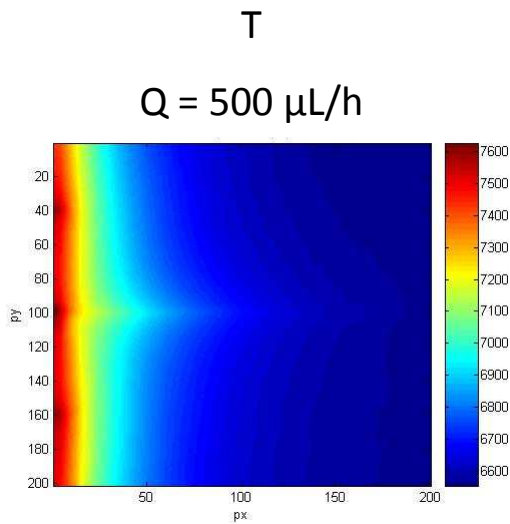
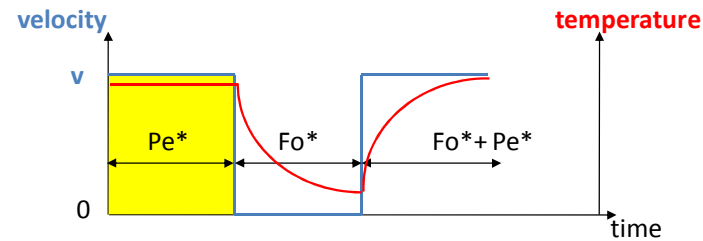
$$St_{i,j}^k = \frac{\sum_{k=n}^{n+Nt} \Delta T_{i,j}^k \cdot Tt_{i,j}^k}{\sqrt{(\sum_{k=n}^{n+Nt} \Delta T_{i,j}^k)^2} \cdot \sqrt{(\sum_{k=n}^{n+Nt} Tt_{i,j}^k)^2}} \quad \text{for } n \in [1; (K - Nt)]$$

$$\text{if } St_{i,j} = 1 \quad \left( \frac{1}{Fo^{*k}_{i,j}} \right) = St_{i,j}^k \frac{\sqrt{(\sum_{k=n}^{n+Nt} \Delta T_{i,j}^k)^2}}{\sqrt{(\sum_{k=n}^{n+Nt} Tt_{i,j}^k)^2}}$$

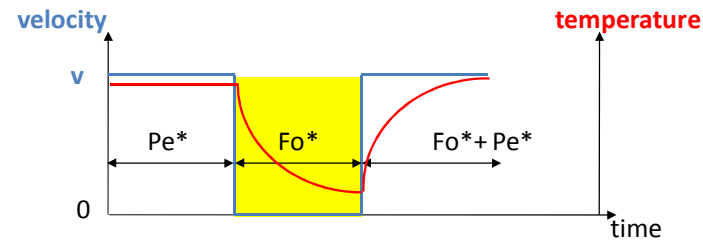


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## Experiment 1 : Steady state



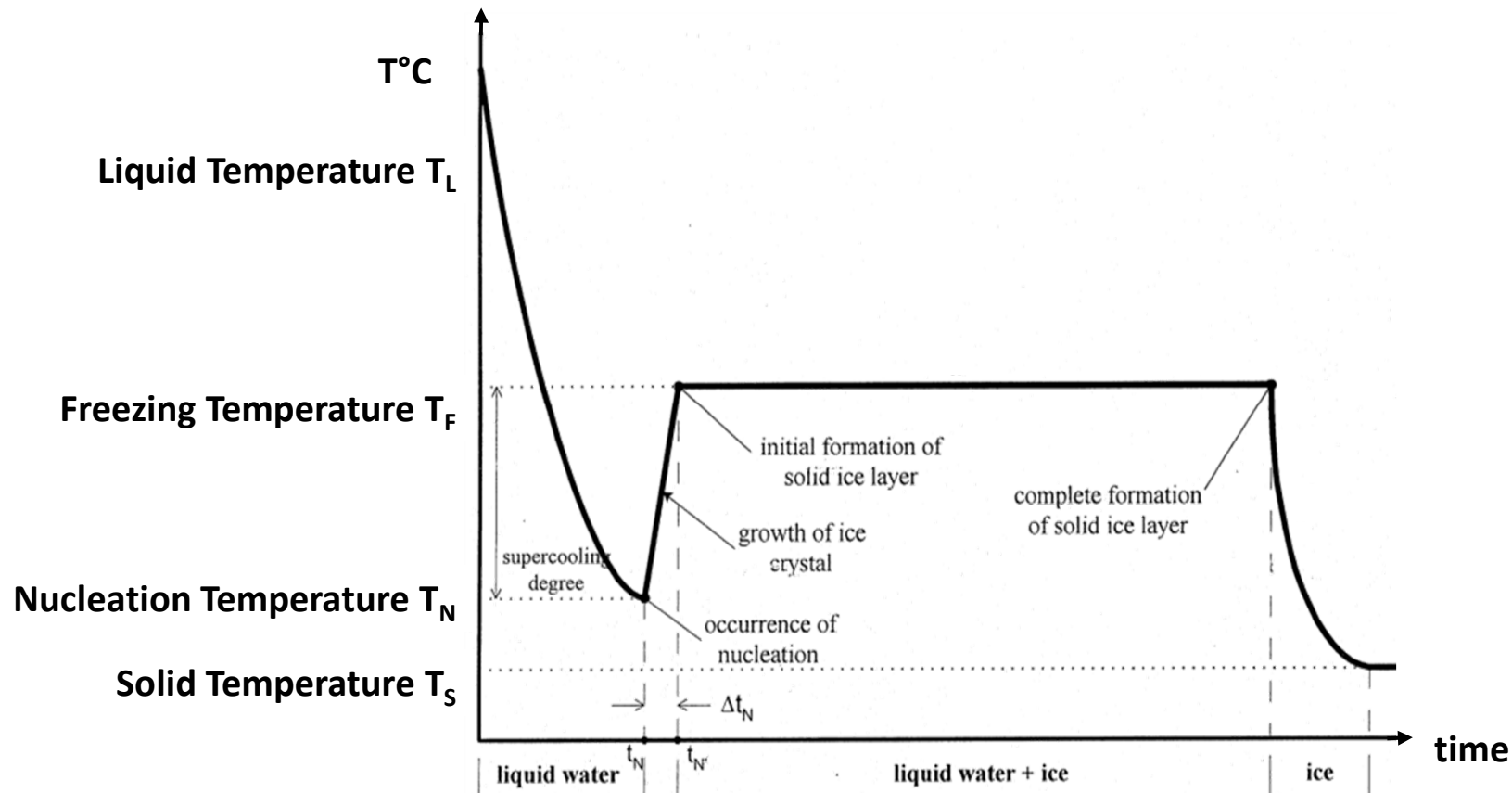
## Experiment 2 : Transient state





## Experiment 3 : Phase change

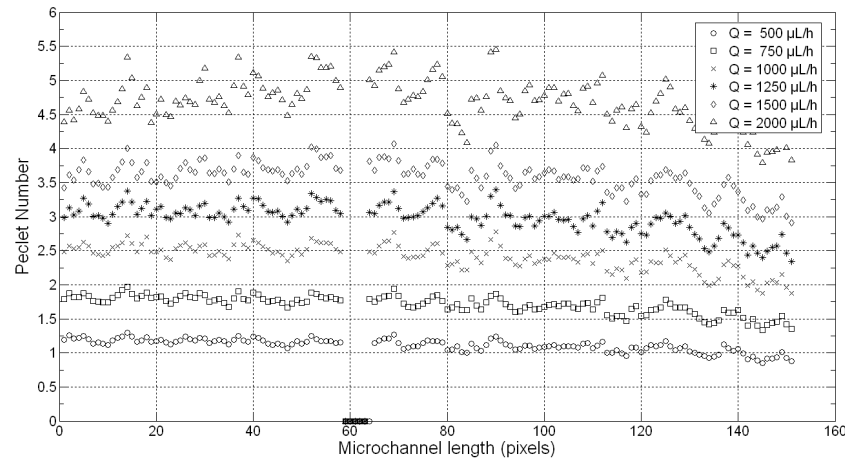
The supercooling theory:



## MATLAB, temperature fields processing

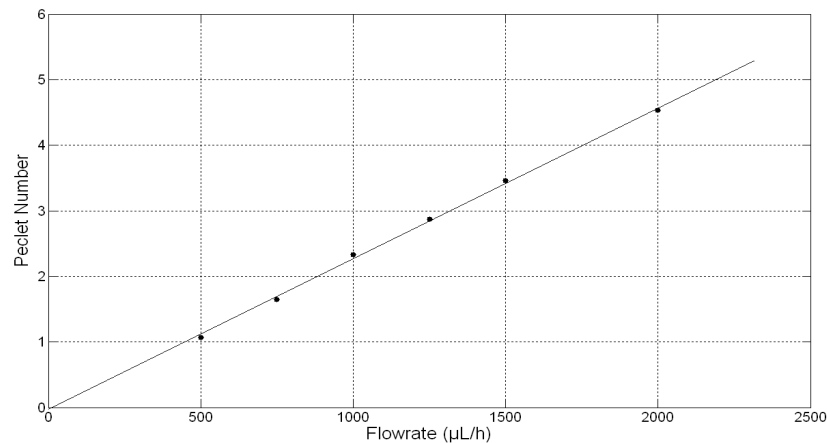
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## Experiment 1: Steady state



-Estimated Peclet number quite stable along the microchannel.

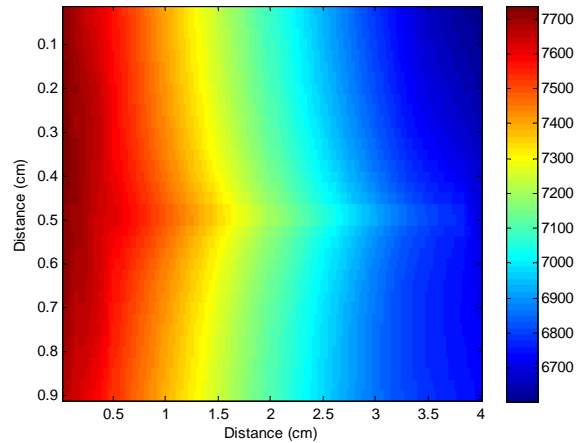
-Higher flow rates are not stable : deformation of PDMS walls



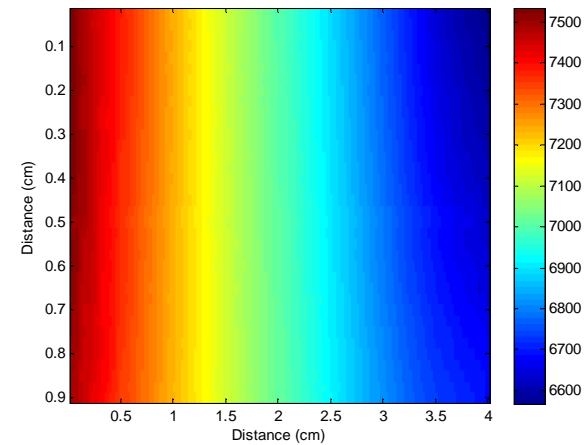
-Linear evolution consistent with physics

## Experiment 2: Transient state

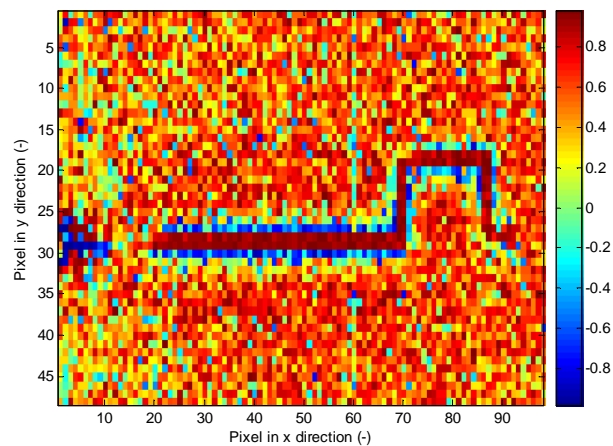
Initial frame



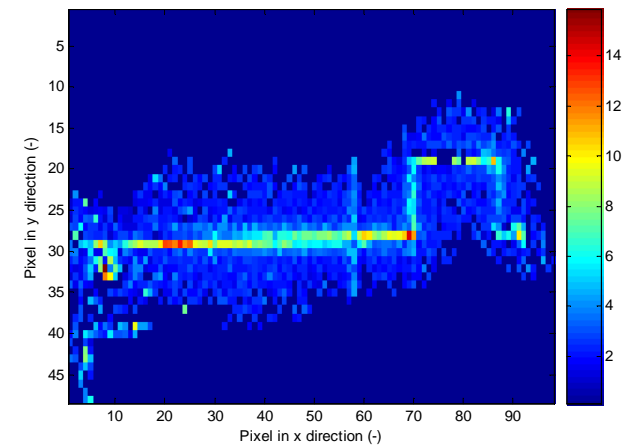
Final frame



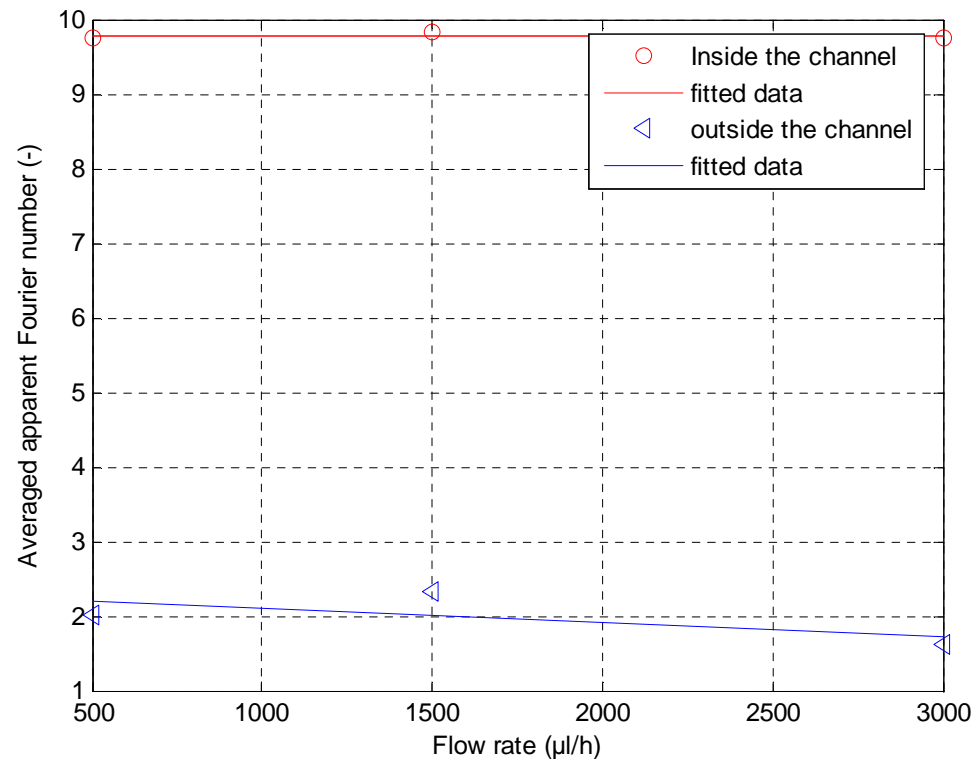
Instant correlation coefficient



Averaged estimated Fo mapping

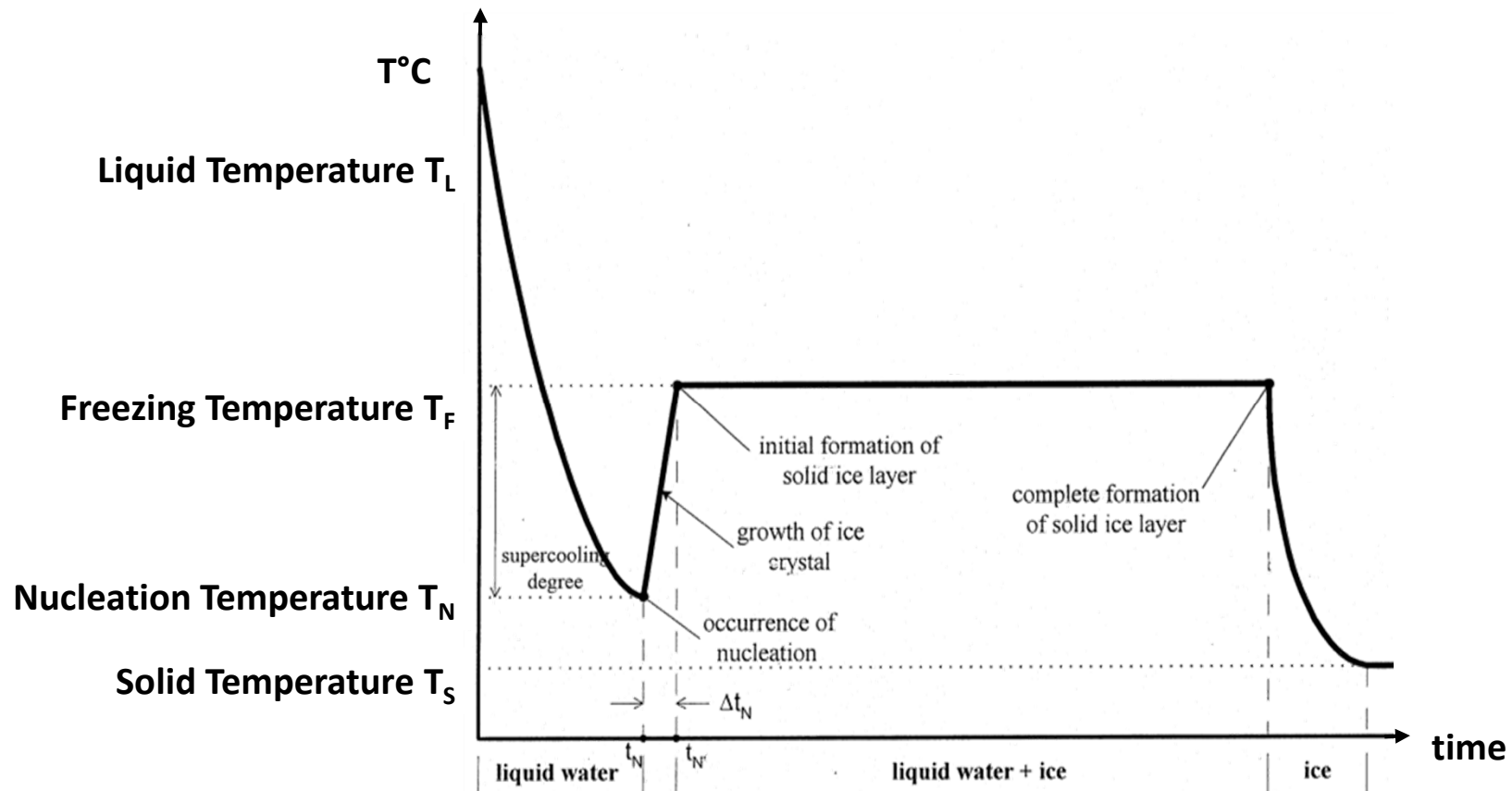


## Experiment 2: Transient state



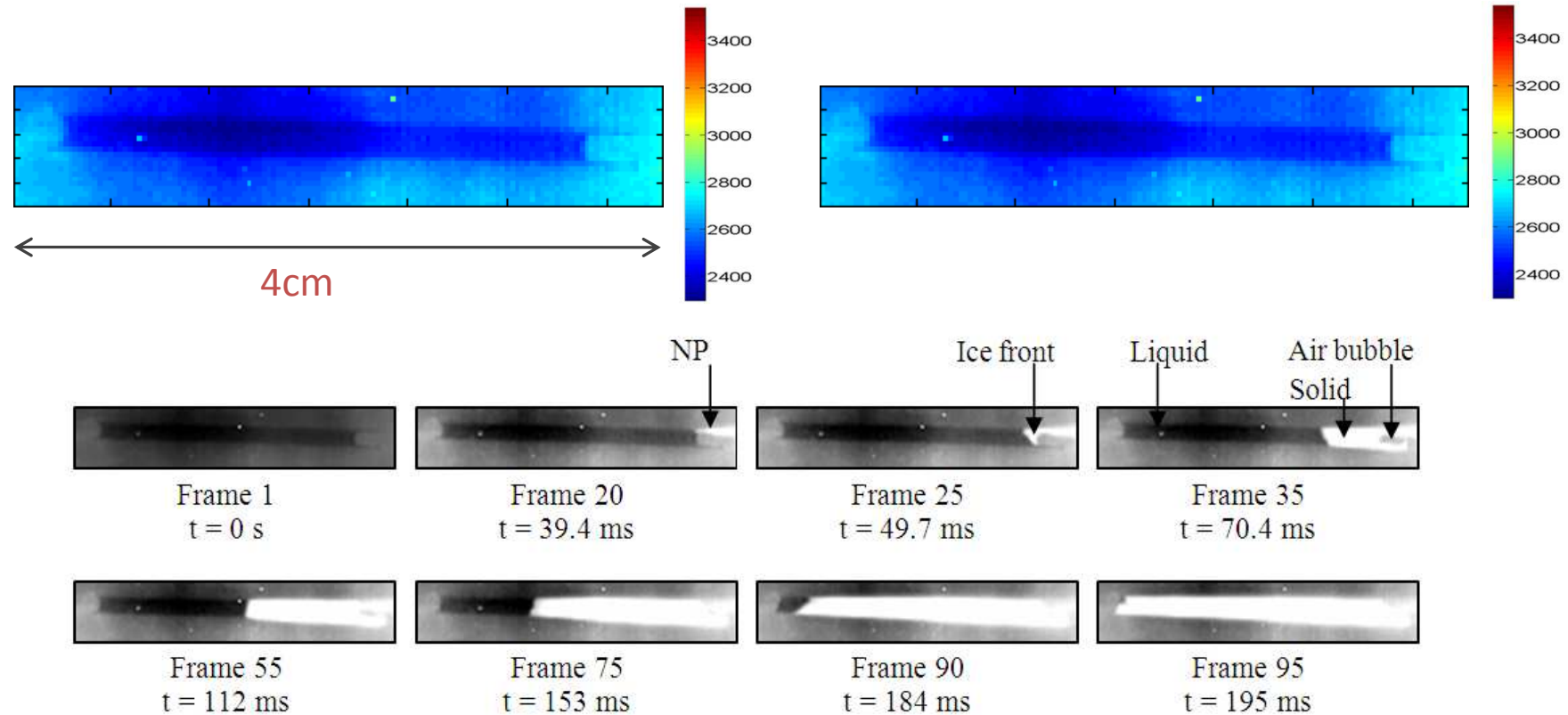
- Estimated Fo number not affected by the flow rate.
- Difference between inside (water+glass) and outside (PDMS+glass) the microchannel.

## Experiment 3: Phase change



## Experiment 3: Phase change

High frequency recordings : 484 Hz

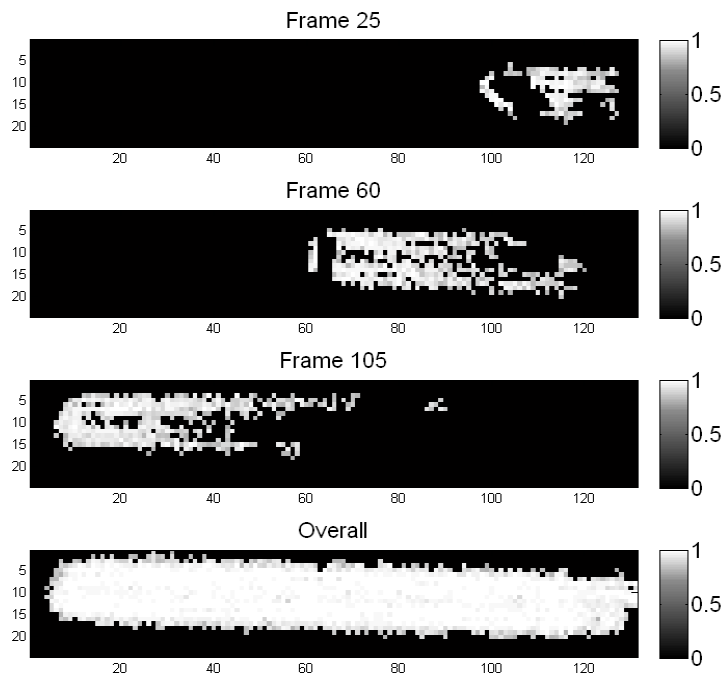


**Question:** How can we localize the heat source ?

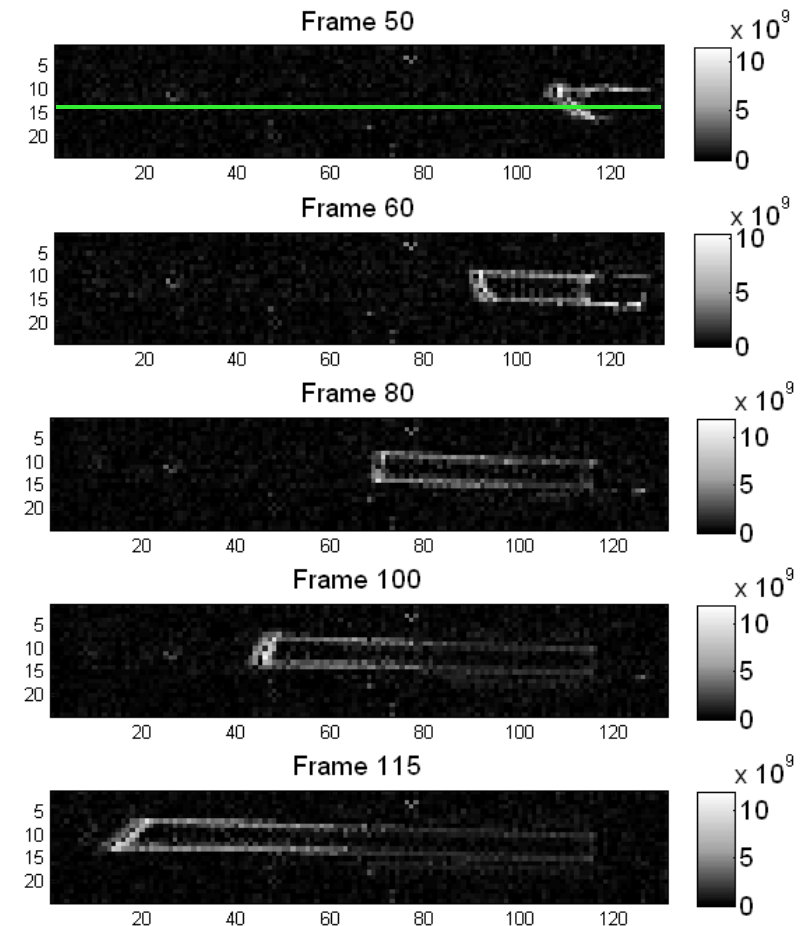


## Experiment 3: Phase change

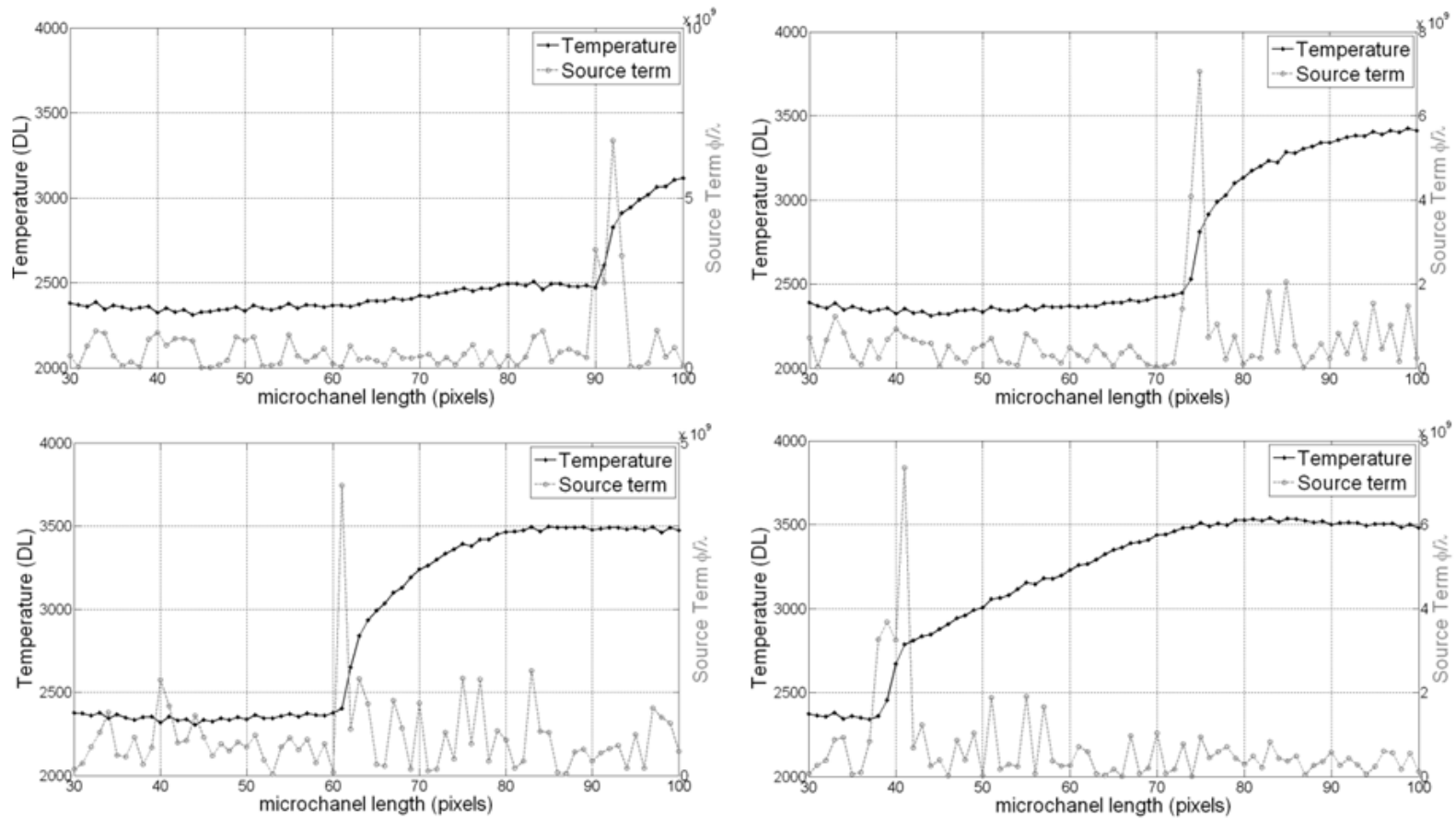
### Correlation coefficient



### Estimation of source term



## Experiment 3: Phase change



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## The correlation method

### Advantages :

- Simple and fast processing
- No calibration of temperature is needed (temperature variations)
- IR Thermography => mapping of estimated parameters
- Large field of applications (chemistry, crystallization, blood flows...)

### Drawbacks:

- Qualitative method (for the moment)

### Perspectives:

- Reduction of noise and filtering of signal (spatial and temporal)
  - SVD + convolution and/or lowpass
- Quantitative estimations
- Improvement of derivations

# Inverse problems in a microchannel

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C. Ravey , C.Pradere



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